IN THE CLAIMS:

1. (currently amended) A process for preparing 3-amino-4,4,4-trifluoro-crotonic esters of the formula (I) or the E/Z isomers or tautomeric forms thereof

or the E/Z-isomers or tautomeric forms thereof wherein

where

 R^1 and R^2 are each independently hydrogen, an optionally substituted linear C_1 - C_4 -alkyl radical or an optionally substituted benzyl radical

and

R³ is methyl or ethyl, comprising

characterized in that

a) reacting an alkyl trifluoroacetate is reacted with an alkyl acetate of the formula CH_3 -CO- OR^3 and an alkali metal alkoxide to give an enolate of a trifluoroacetoacetic ester of the formula (II)

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(II)

where wherein

M = Na or K

and

R³ is as defined above,

and subsequently

- b) allowing reacting the alkali metal enolate of the trifluoroacetoacetic ester from stage a) without further purification is allowed to react directly with an amine of the formula NHR¹R², where R¹ and R² are each as defined above, in the presence of an acid to provide give the 3-amino-4,4,4-trifluorocrotonic ester.
- 2. (currently amended) The process of claim 1, characterized in that wherein said the alkyl trifluoroacetates and alkyl acetates used are the corresponding methyl or ethyl esters.
- 3. (currently amended) The process of claim 1, wherein or 2, characterized in that, in stage a), the molar ratio of alkyl trifluoroacetate to alkyl acetate is set to from 1:1 to 1:5.

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- 4. (currently amended) The process according to any of claims claim 1, wherein to 3, characterized in that, from 0.9 to 3.0 mol of the alkali metal alkoxide are present used per mole of alkyl trifluoroacetate.
- 5. (currently amended) The process of claim 1, wherein any of claims 1 to 4, characterized in that the alkali metal alkoxide used is selected from the group consisting of sodium methoxide, sodium ethoxide, potassium methoxide and or potassium ethoxide.
- 6. (currently amended) The process of claim 1, wherein any of claims 1 to 5, characterized in that the reaction in stage a) is carried out at temperatures a temperature of from 0 to 100°C.
- 7. (currently amended) The process of claim 1, further comprising removing any of claims 1 to 6, characterized in that, on completion of stage a), excess alkyl acetate and/or alcohol upon completion of stage a) is removed.
- 8. (currently amended) The process of claim 1, wherein any of claims 1-to 7, characterized in that the amine NHR 1R2 is used in stage b) is as a free base in anhydrous form.
- 9. (currently amended) The process of any of claims 1 to 7, characterized in that claim 1, wherein the amine NHR 1R2 is used in stage b) is an in aqueous solution.
- 10. (currently amended) The process of claim 1, wherein any of claims 1 to 7, characterized in that the amine NHR¹R² is used in stage b) is in the form of a salt selected from the group consisting of hydrochloride, sulfate, nitrate, formate and or acetate.
- 11. (currently amended) The process of claim 1, wherein any of claims 1 to 10, characterized in that the amine NHR¹R² used is selected from the group consisting of ammonia, methylamine, ethylamine, benzylamine, dimethylamine and or diethylamine, or a salt of these amines.

- 12. (currently amended) The process of claim 1, wherein any of claims 1 to 11, characterized in that from 1.0 to 10.0 mol mol, in particular from 1.1 to 4.0 mol, of amine are is provided used per mole of alkyl trifluoroacetate.
- 13. (currently amended) The process of claim 1, wherein any of claims 1 to 12, characterized in that the acid is used in stage b) is present in an amount of from 1.0 to 10.0 mol per mole of alkyl trifluoroacetate.
- 14. (currently amended) The process of claim 1, wherein any of claims 1 to 13, characterized in that the acid used is acetic acid and/or hydrochloric acid.
- 15. (currently amended) The process of claim 1, wherein any of claims 1 to 14, characterized in that reaction stage b) is carried out at temperatures of from 20 to 200°C 200°C, in particular from 50 to 160°C.
- 16. (currently amended) The process of claim 1, wherein any of claims 1 to 15, characterized in that the water of reaction is removed continuously during the reaction of stage b).
- 17. (currently amended) The process of claim 1, wherein any of claims 1 to 16, characterized in that the reaction of stage b) is carried out in the presence of an organic hydrocarbon as an azeotroping agent.
- 18. (currently amended) The process of claim 1, wherein any of claims 1 to 17, characterized in that the azeotroping agent used is a solvent selected from the group consisting of hexane, octane, cyclohexane, methylcyclohexane, benzene, toluene and a xylene or the xylenes.
- 19. (currently amended) The process of claim 1, wherein any of claims 1 to 18, characterized in that the reaction mixture is worked up by extraction and subsequent distillation.

- 20. (currently amended) The process of claim 1, wherein any of claims 1 to 19, characterized in that stages a) and b) are carried out successively in the same reaction vessel.
- 21. (new) The process of claim 1, wherein from 1.1 to 4.0 mol of amine is provided per mole of alkyl trifluoroacetate.
- 22. (new) The process of claim 1, wherein reaction stage b) is carried out at temperatures of from 50 to 160°C.